



中国科学院过程工程研究所

Institute of Process Engineering, Chinese Academy Of Sciences

敬业 团结 求实 创新

**2017 NETL Workshop on Multiphase Flow**



# **Statistical Analysis on Large-scale Direct Numerical Simulation of Gas-solid Flow**

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**Morgantown, WV · 2017.8.8**

# Outline



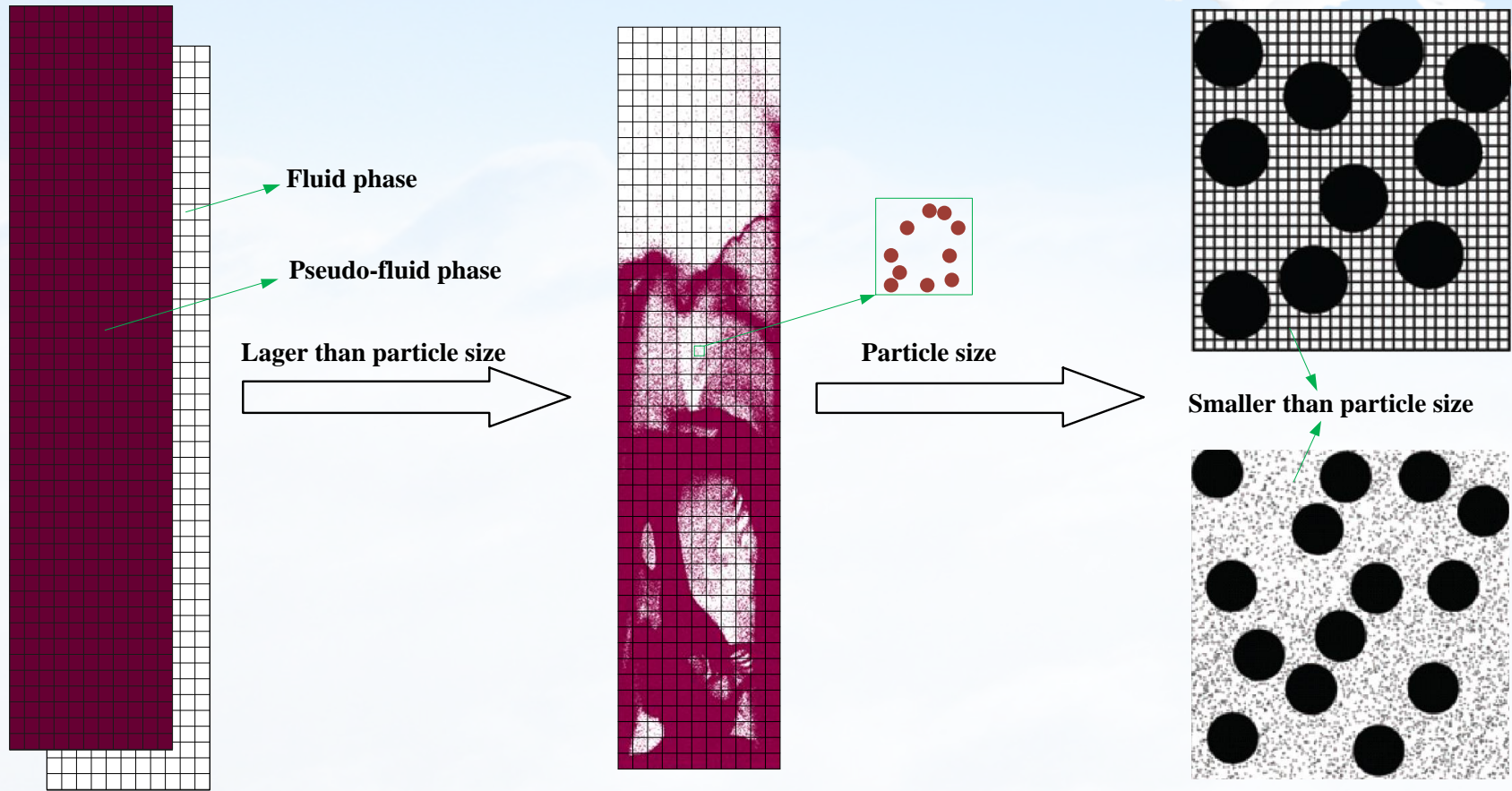
- **Background**

- **Enabling Large-scale DNS**

- **Numerical Results**

- **Conclusions**

# Multi-scale Modelling for Gas-solid Flow

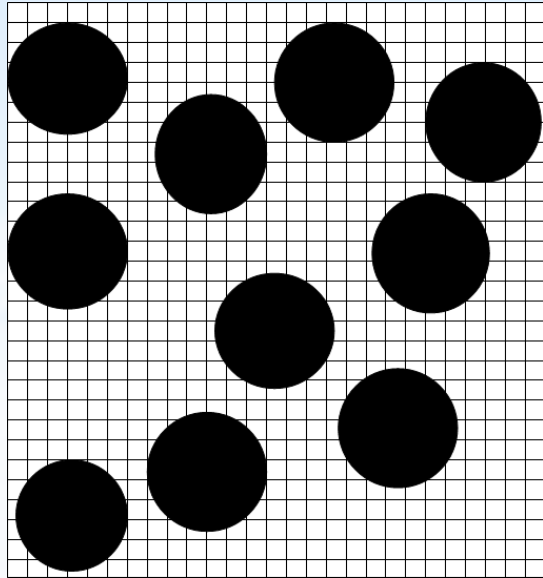


**Two-fluid Model  
(TFM)**

**Discrete Particle Model  
(DPM or CFD-DEM)**

**Direct Numerical Simulation  
(DNS)**

# Particle-resolved DNS



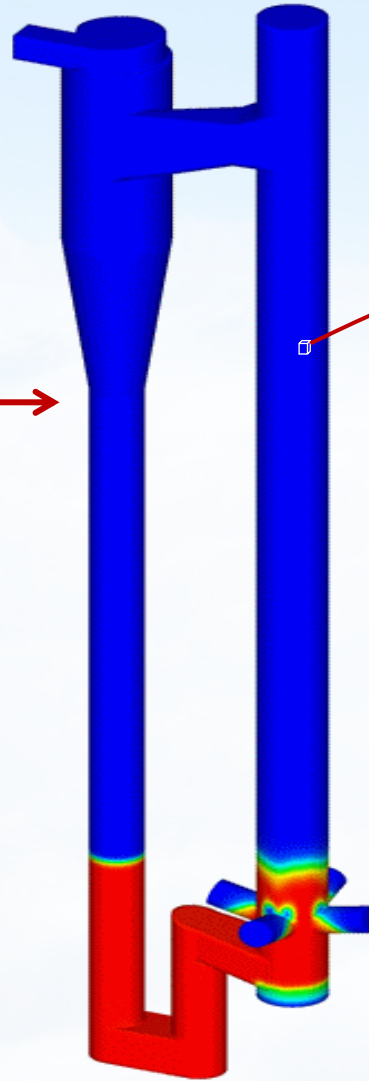
Computational grid  $h \ll d_p$  Particle diameter

The mesh is reduced to below the size of particle, and the flow field around particle is fully resolved. The fluid-solid interaction force is directly obtained by integrating the viscous stress on the surface of the particles.

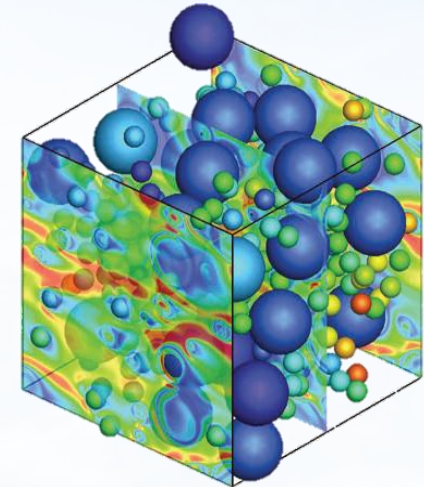
DNS can be regarded as the most accurate method, but its huge computational cost leads to small-scale simulation domain



# DNS VS Real Constitutive Laws



Real gas-solid flows  
A computational grid  
 $N_p \sim O(10^5)$

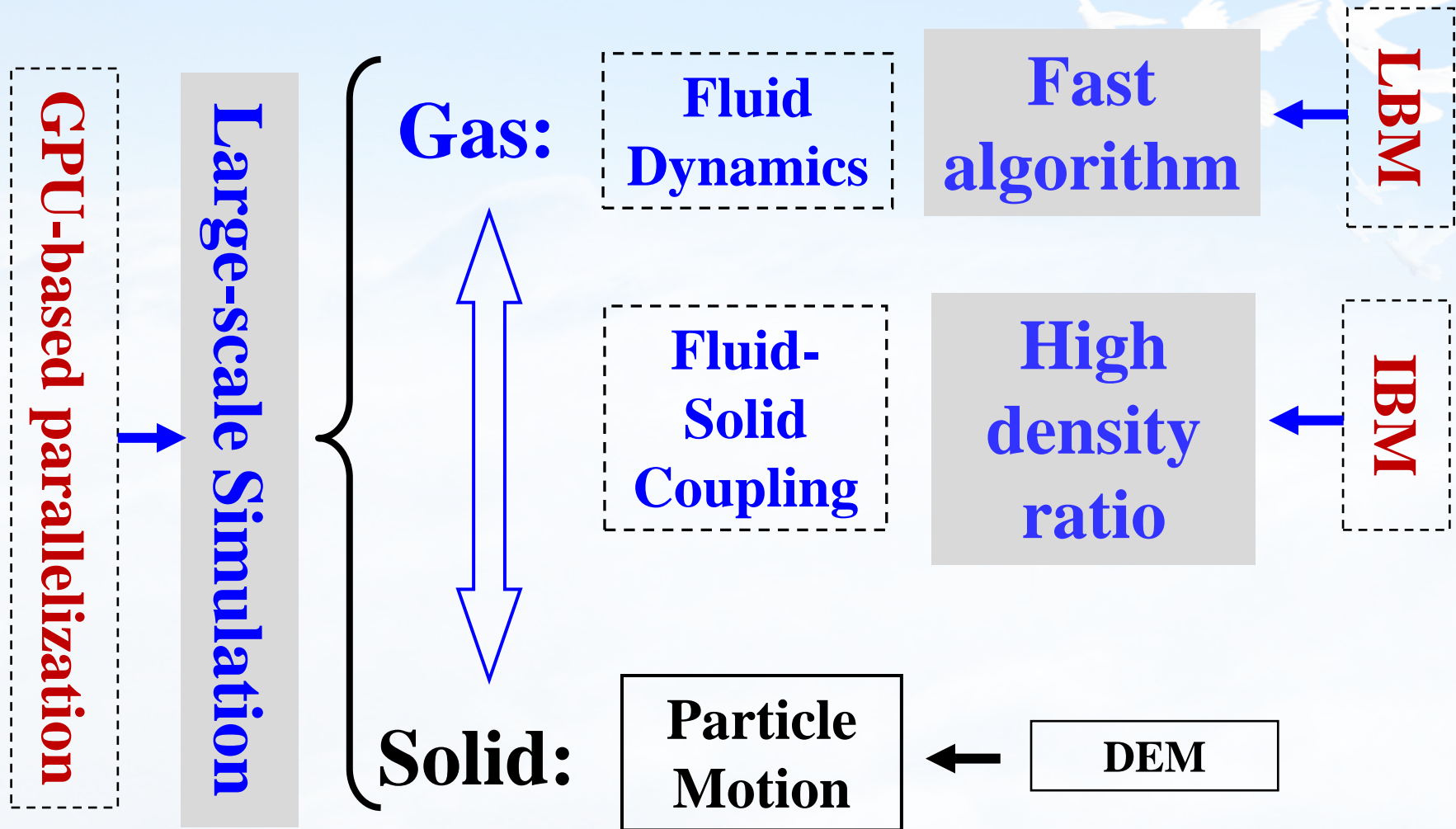


(S Tenneti , S Subramaniam. *Annu. Rev. Fluid Mech.* 2014, 46:277-286)

**Particle-resolved DNS**

$N_p \sim O(10^2)$

# Strategies for Enabling Large-scale DNS



# Outline

- **Background**



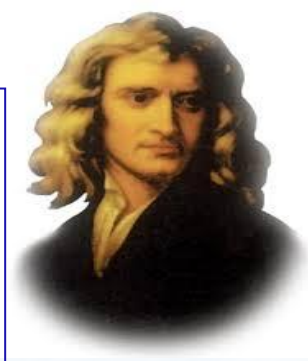
- **Enabling Large-scale DNS**

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# Discrete Modeling of Particle-Fluid System

Particle

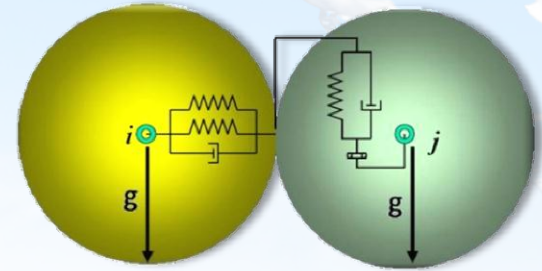


Issac Newton  
(1643.1.4-1727.3.31)

Newton's  
second law

$$\mathbf{F} = m\mathbf{a}$$

Inter-particle collision



Gas



Ludwig Edward Boltzmann  
(1844.2.20-1906.9.5)

Boltzmann equation

$$\frac{Df}{Dt} = \frac{\partial f(t, \mathbf{x}, \mathbf{v})}{\partial t} + \mathbf{v} \frac{\partial f(t, \mathbf{x}, \mathbf{v})}{\partial \mathbf{x}} = \Omega$$

Discrete form

$$f(\mathbf{x} + \mathbf{e}_i \Delta t, t + \Delta t) - f(\mathbf{x}, t) = \Omega_i$$



# Improved Solution for Gas Flow

Navier-stokes equation

$$\rho \frac{d\mathbf{u}}{dt} = -\nabla p + \mu \Delta \mathbf{u} + \rho g$$

**Implicit, Serial, Euler**



**parallelization**

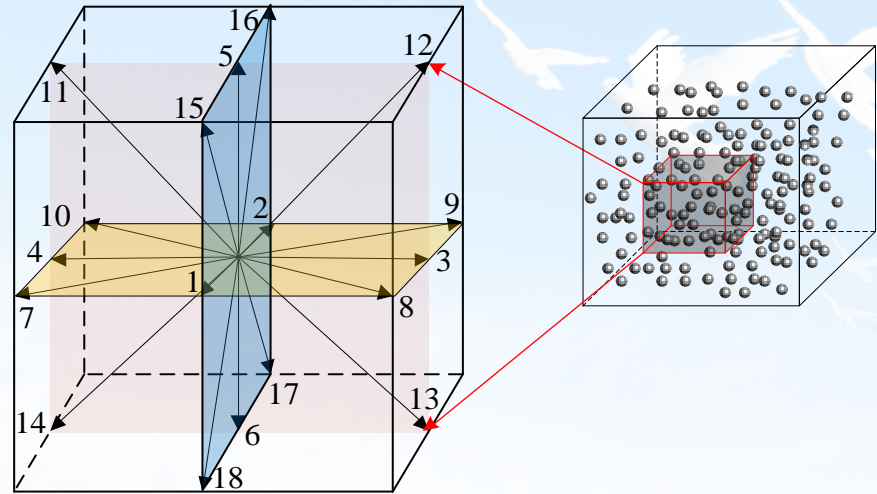
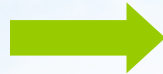
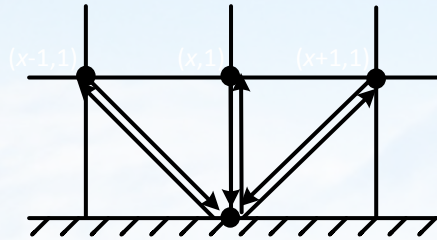
Lattice Boltzmann equation

$$f(\mathbf{x} + \mathbf{e}_i \Delta t, t + \Delta t) - f(\mathbf{x}, t) = \Omega_i$$

**Explicit, Parallel, Lagrange**

# Lattice Boltzmann method

Simple rule:  
bounce-back boundary condition



**Molecular Model**

**Boltzmann eq.**

**Collisionless Boltzmann eq..**

**Continuous Model**

**Euler eq.**

**Navier—Stokes eq.**

**Conservation eq. is not closed**

$$Kn = \frac{\bar{\lambda}}{L}$$

→ 0

0.01

0.1

1

10

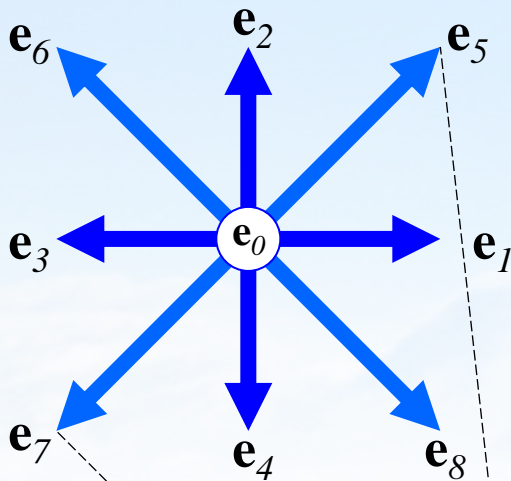
100

→ +∞

Inviscid flow

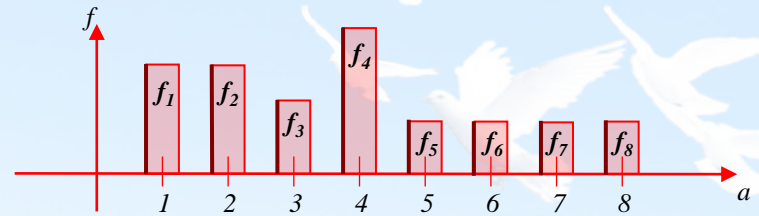
Free molecular flow

# Collision and Streaming Steps

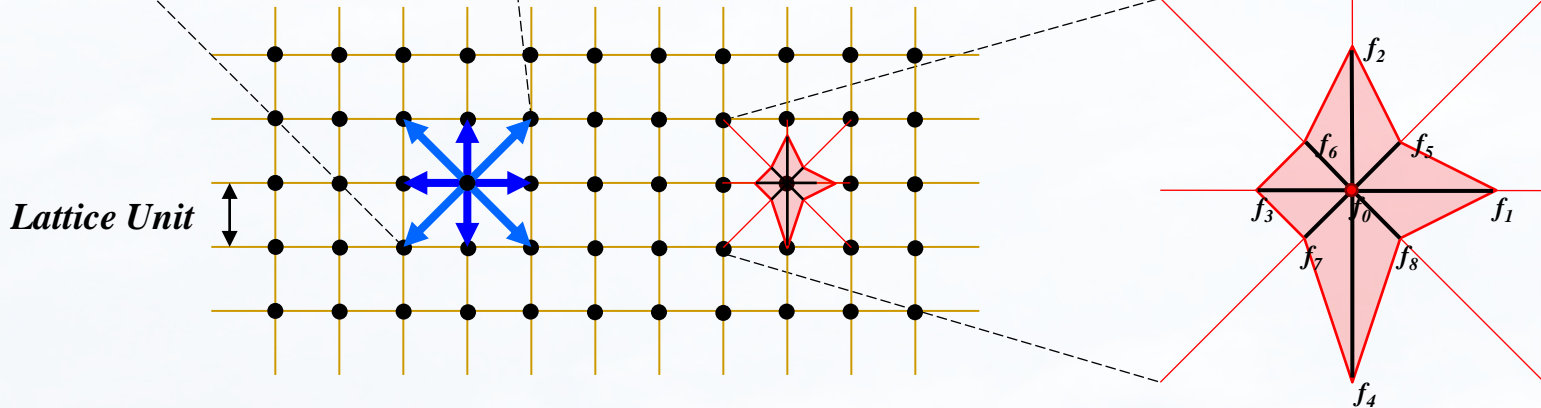


D2Q9 model

D3Q19 model



Histogram view of the distribution function,  $f$ .

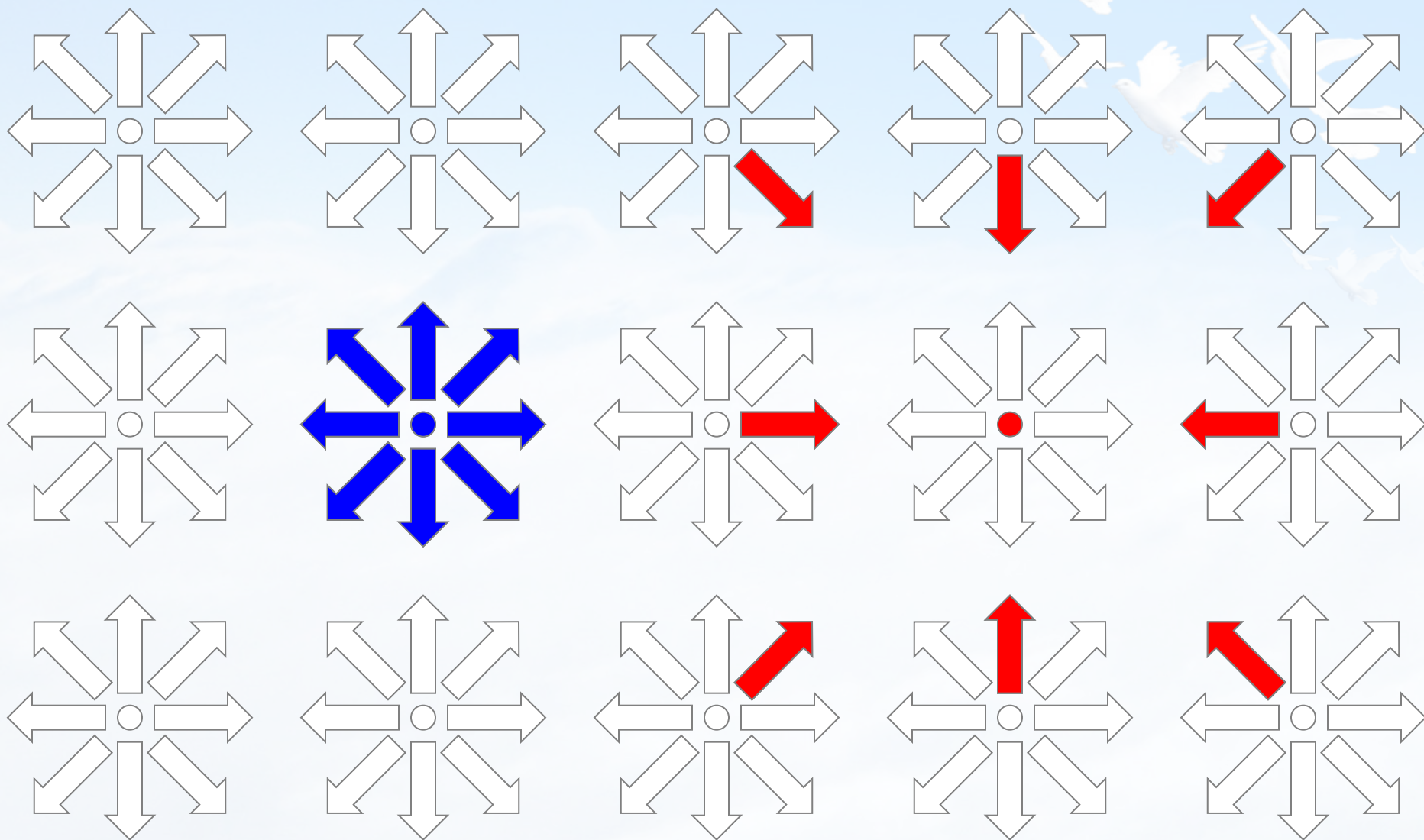


Discrete velocities  $e_i$   
Directional densities  $f_i$



Macroscopic velocity  $u = \frac{1}{\rho} \sum_i e_i f_i$   
Macroscopic density  $\rho = \sum_i f_i$

# Streaming step $f_i(x + e_i \delta_t, t + \delta_t) = f_i^*(x, t)$

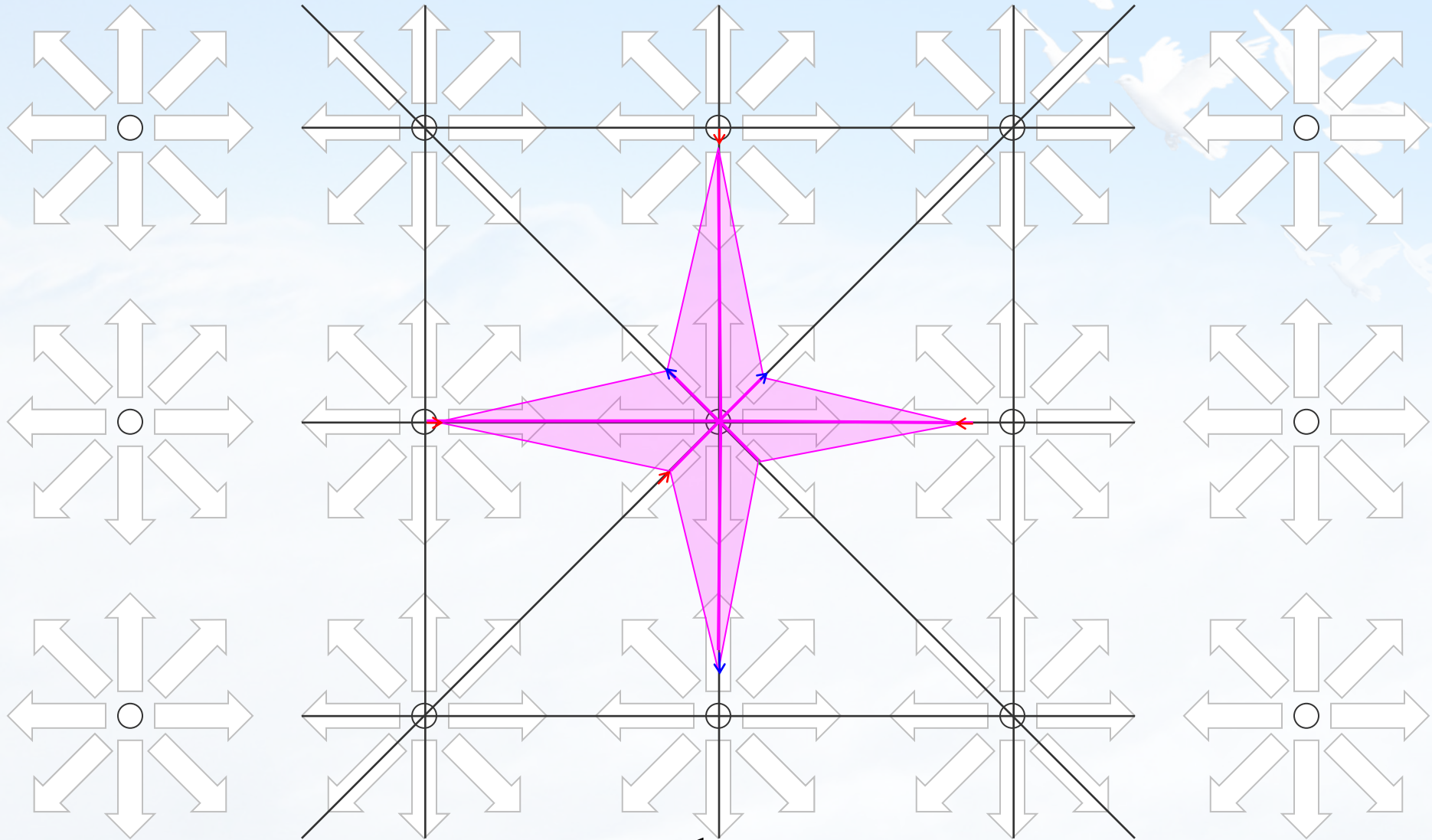


(a) From the node to its neighboring nodes

(b) From the neighboring nodes to local node

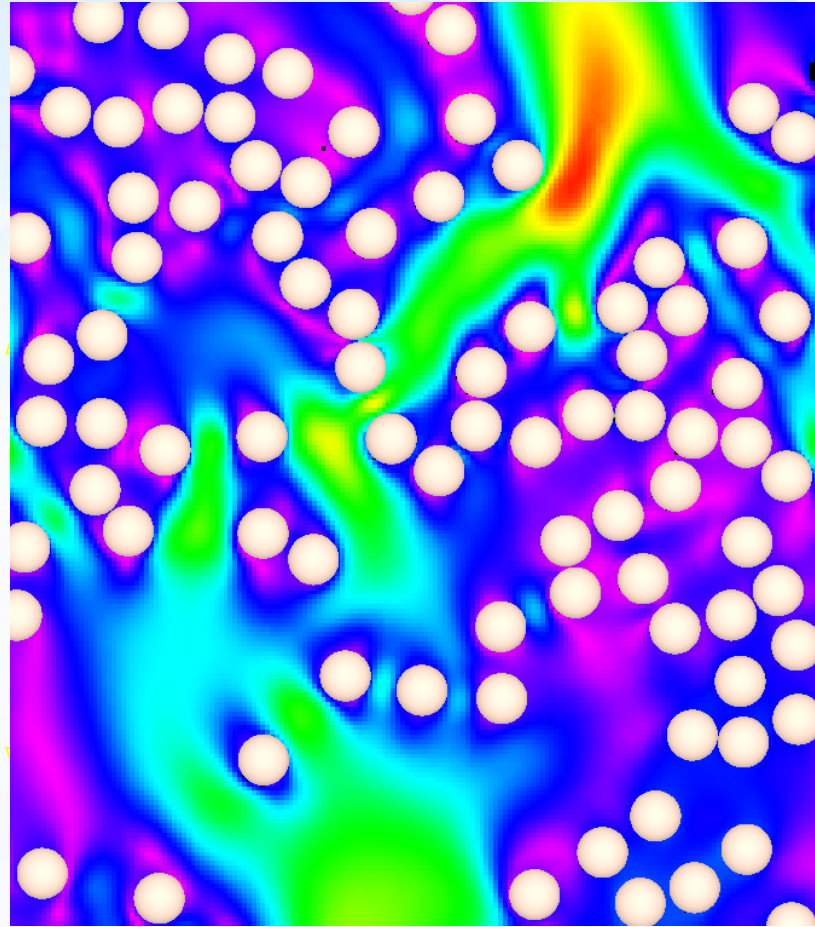


# Collision step $f_i^*(x, t) = f_i(x, t) + \frac{1}{\tau} [f_i^{eq}(x, t) - f_i(x, t)]$



Calculate  $f_i^* = f_i + \frac{1}{\tau} [f_i^{eq} - f_i]$

# Computation's Speedup 3000x



Traditional algorithm: 1024 particles, 1024CPU takes one month  
New algorithm: 1400 particles, single CPU takes 7 days!

# Immersed Boundary Method

$$f_i(\mathbf{x} + \mathbf{e}_i \Delta t, t + \Delta t) = f_i(\mathbf{x}, t) + \frac{1}{\tau} (1 - \beta(\varepsilon_s, \tau)) (f_i^{eq}(\rho, \mathbf{v}) - f_i(\mathbf{x}, t)) + \beta(\varepsilon_s, \tau) \Omega_i^s$$

Weighting function

Weighting function

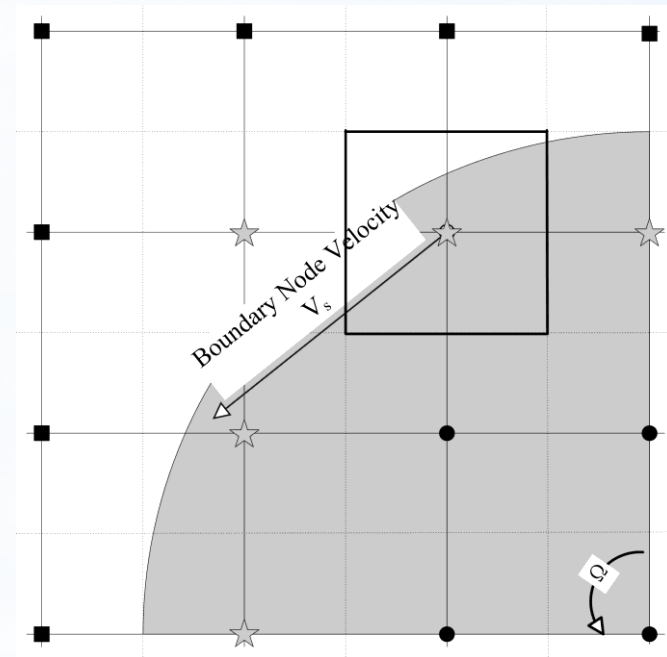
Additional collision term

$$\beta(\varepsilon_s, \tau) = \frac{\varepsilon_s (\tau - 0.5)}{(1 - \varepsilon_s) + (\tau - 0.5)}$$

Additional collision term

$$\Omega_i^s = f_{-i}(\mathbf{x}, t) - f_i(\mathbf{x}, t) + f_i^{eq}(\rho, \mathbf{V}_s) - f_{-i}^{eq}(\rho, \mathbf{v})$$

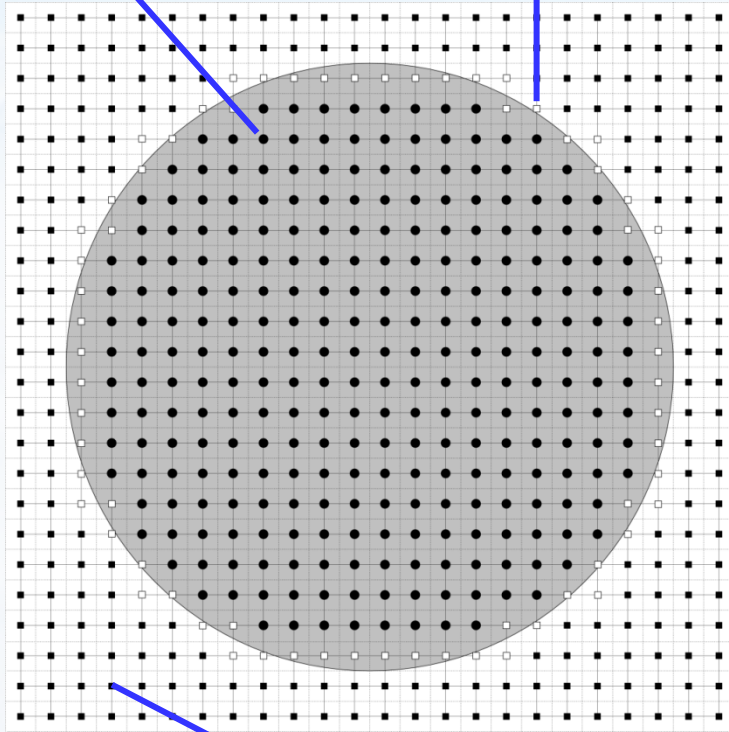
Solid volume fraction  $\varepsilon_s = \frac{V_{solid}}{V_{cell}}$



# Fluid-structure Interactions

Interior solid  
node

Boundary  
node



Fluid node

Force acting on particle:

$$\mathbf{F}_{f \rightarrow p} = \frac{h^2}{\Delta t} \sum_{j=1}^n \left( \beta_j \sum_{i=1}^8 \Omega_i^s \mathbf{e}_i \right)$$

Fluid-induced torque:

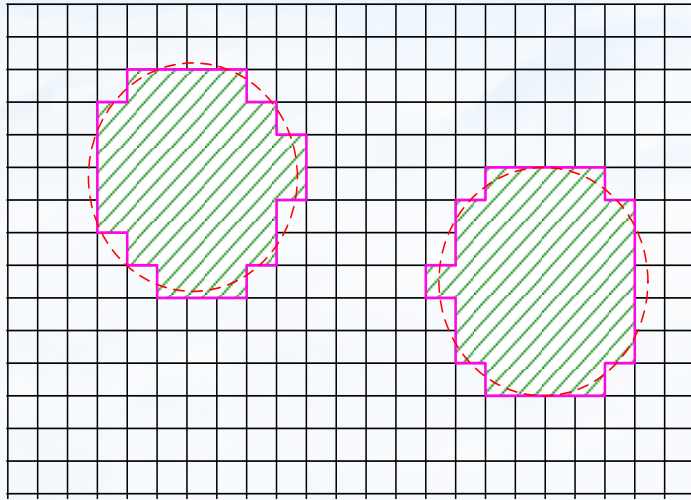
$$\mathbf{T}_{f \rightarrow p} = \frac{h^2}{\Delta t} \sum_{j=1}^n \left( (\mathbf{x}_j - \mathbf{x}_c) \times \beta_j \sum_{i=1}^8 \Omega_i^s \mathbf{e}_i \right)$$



# Enhance Stability of Parallel Algorithm

**Traditional link-based LBM method**  
(Ladd A.J.C., *J. Fluid Mech.* 1994,271:311-339)

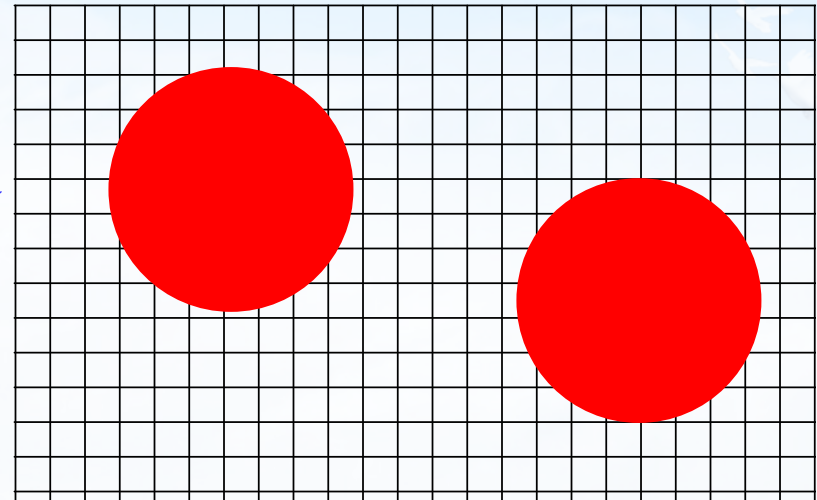
**Our proposed LBM-DEM method**



**Gas-solid**

$\Delta t < 10^{-8}s$

Stability  
➔



$\Delta t \sim 10^{-6}s$

**Time step by 100 times**

# Large-scale GPU Parallel Computing

**Mole-8.5** (born on April 24)

2P

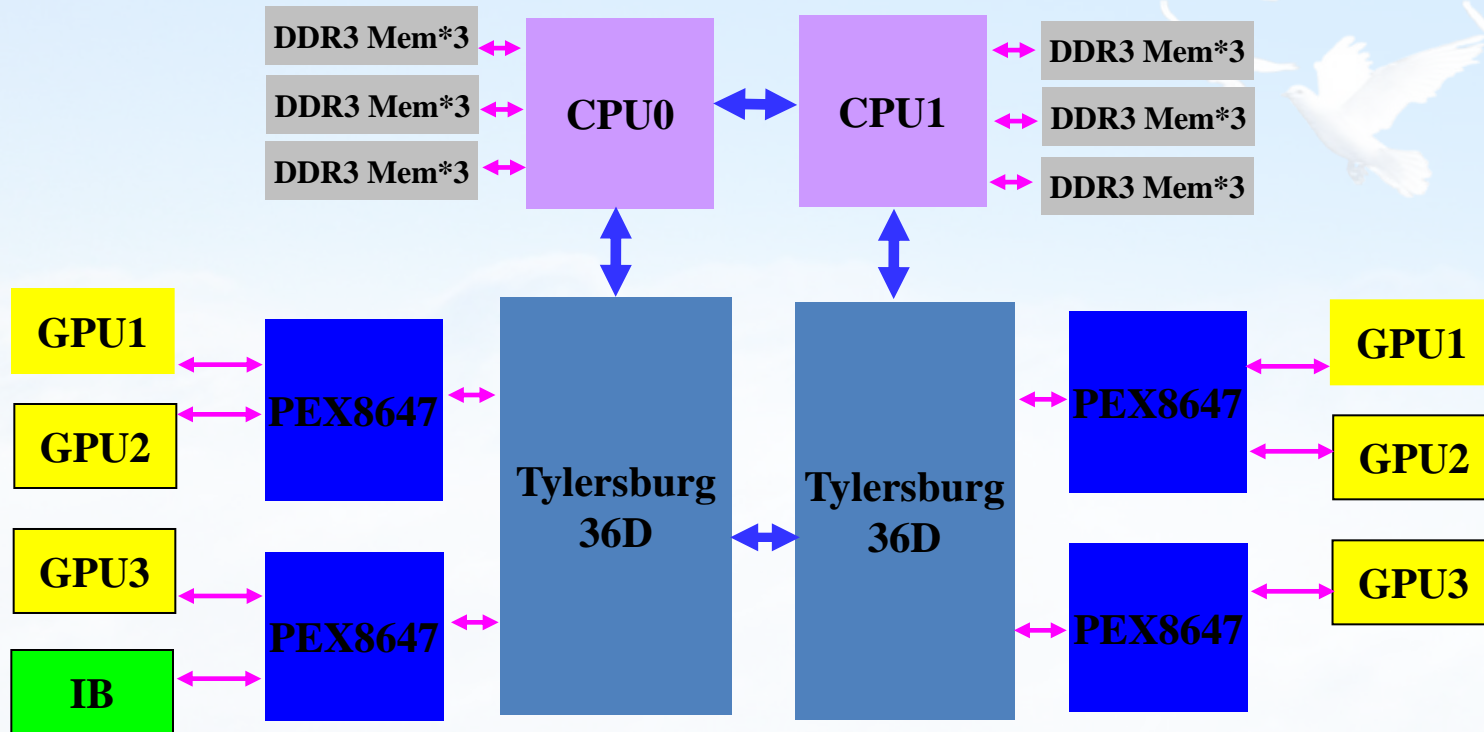


(19<sup>th</sup>, June 2010, Top500)



(9<sup>th</sup>, Nov 2011, Green500)

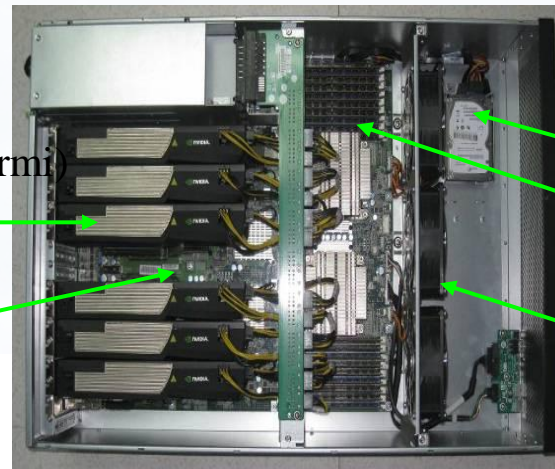
# Node layout of Mole-8.5



6xC2050 (Fermi)

QDR IB

Tyan S7015



HD

Mem

2xE5520/70

Fan

# GPU Parallel Implementation



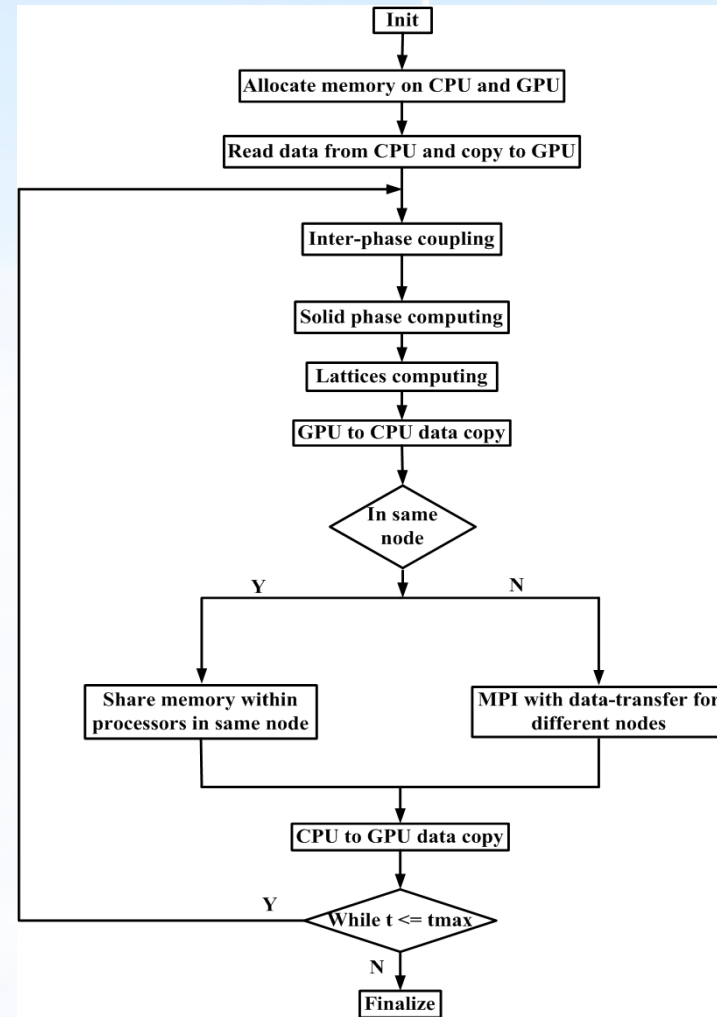
**CPU**

**Center Processing Unit**



**GPU**

**Graphic Processing Unit**



**Flow Chart of GPU implementation**



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# Performance of GPU vs. CPU

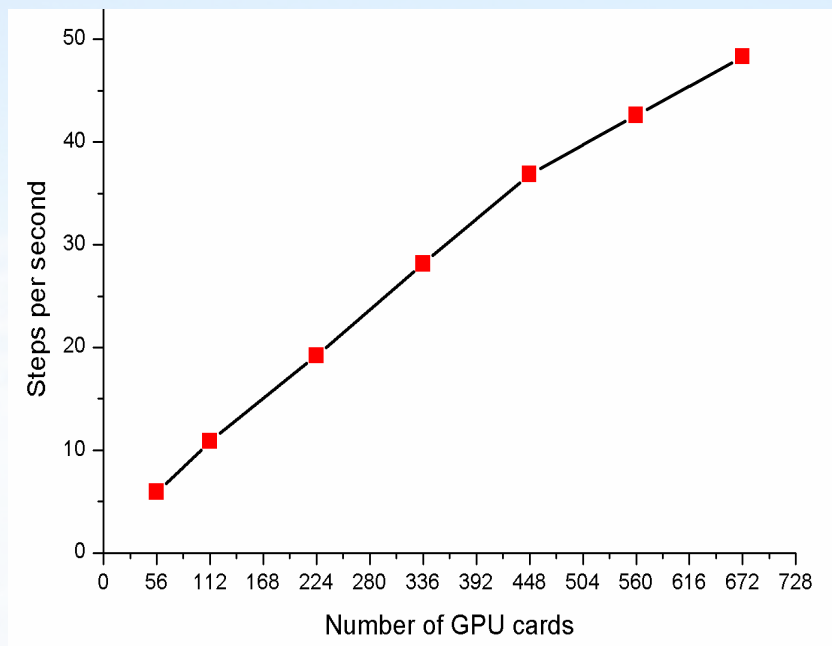
(Single GPU)

D3Q19 LBM-DEM

Domain size (W×H×L)	Steps per second (Fermi GPU)	Steps per second (Intel E5520)	Speedup	Perf. (MLUPS) (double precision)
32×64×32	1784.1	65.71	27.1	116.8
64×64×64	458.6	16.44	27.9	120.2
64×128×64	237.5	8.167	29.1	124.5
128×128×128	60.4	2.043	29.6	126.6
128×256×128	33.3	1.056	31.5	139.8

\*MLUPS: **m**ega-**l**attice-**u**pdates-**p**er-**s**econd

# Performance of Large-scale Simulation



D3Q19 TDHS-LBM

(Multi GPUs)

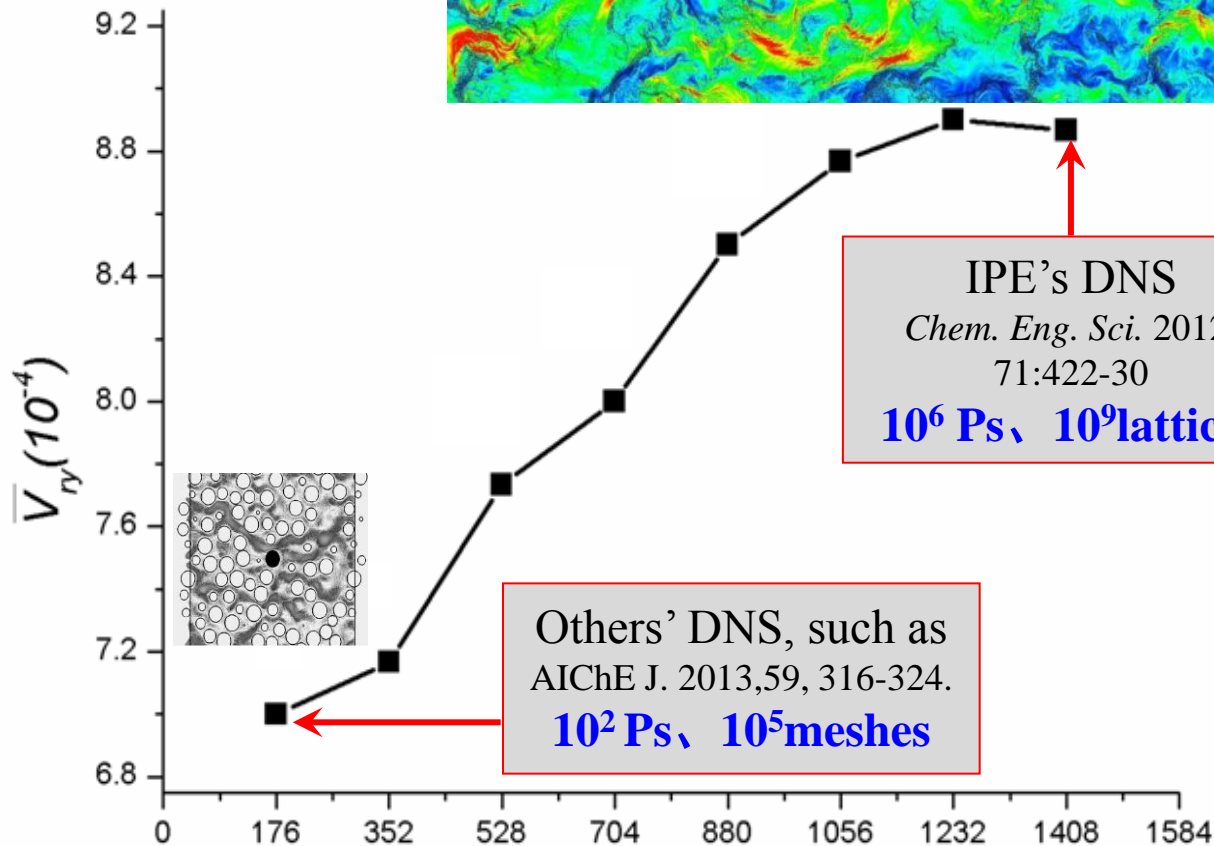
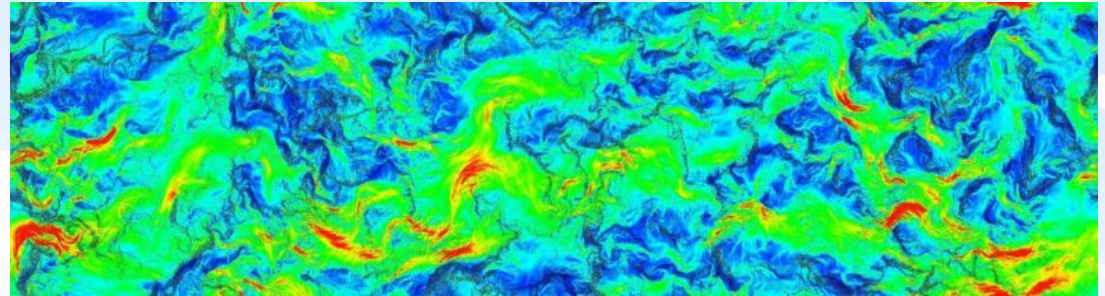
Strong scaling for  
large-scale gas-solid  
simulations on Mole-8.5

Case	Lattice	GPU	Steps	Time	Perf. (MLUPS)	Perf./GPU	Gflops
1	$1024 \times 1152 \times 1024$	$8 \times 8 \times 8$	2000	100.2	24111	47.1	10558
2	$1536 \times 1728 \times 1536$	$12 \times 12 \times 12$	2000	106.2	76741	44.4	33611

The number of float operations per step of case1: 529 Gflop, case2: 1785.6 Gflop

# Largest Scale DNS of Gas-solid Suspensions

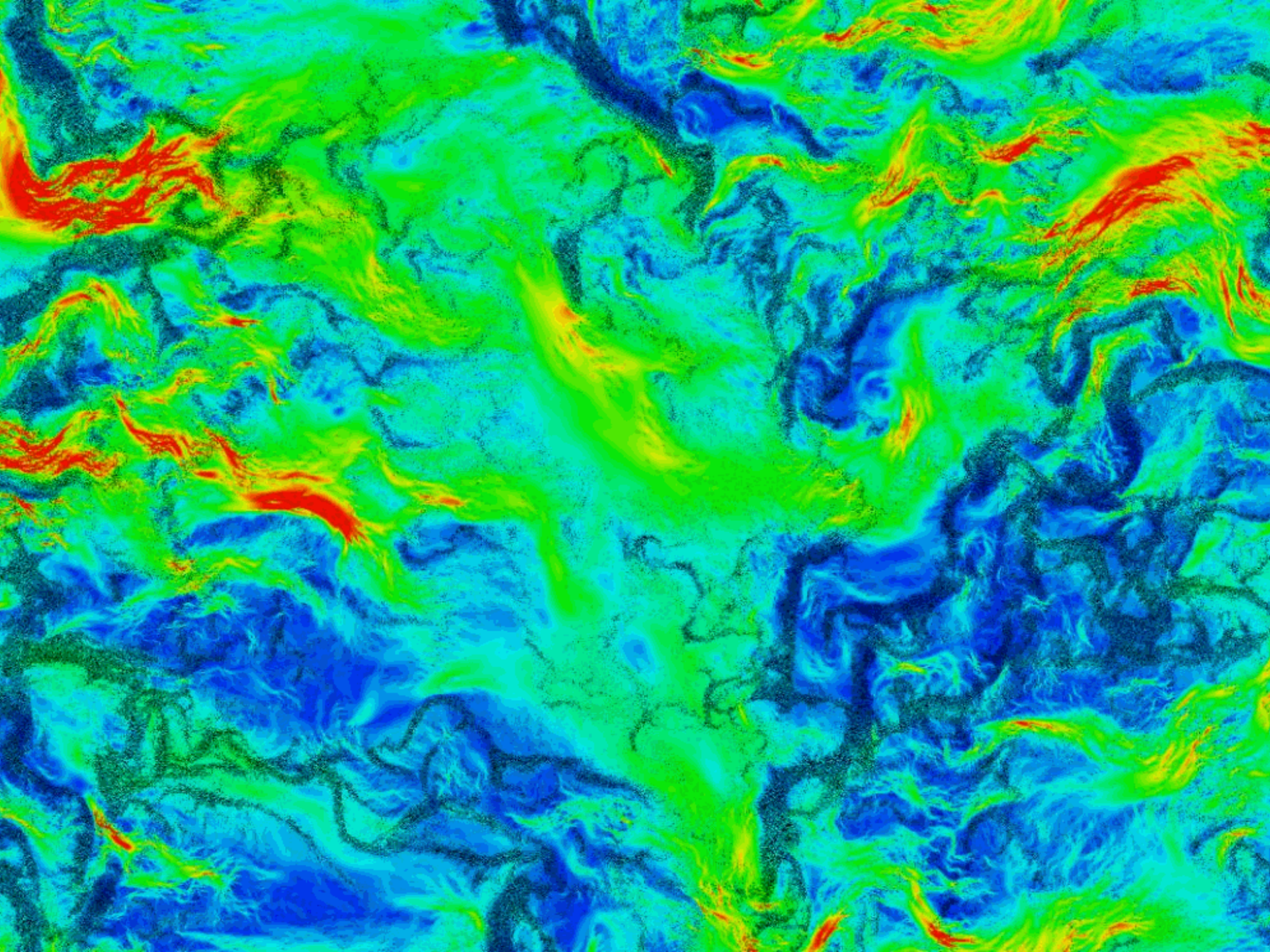
1M solid particles & 1G fluid lattices @ 576 GPUs



IPE's DNS  
*Chem. Eng. Sci.* 2012,  
71:422-30  
**10<sup>6</sup> Ps, 10<sup>9</sup> lattices**

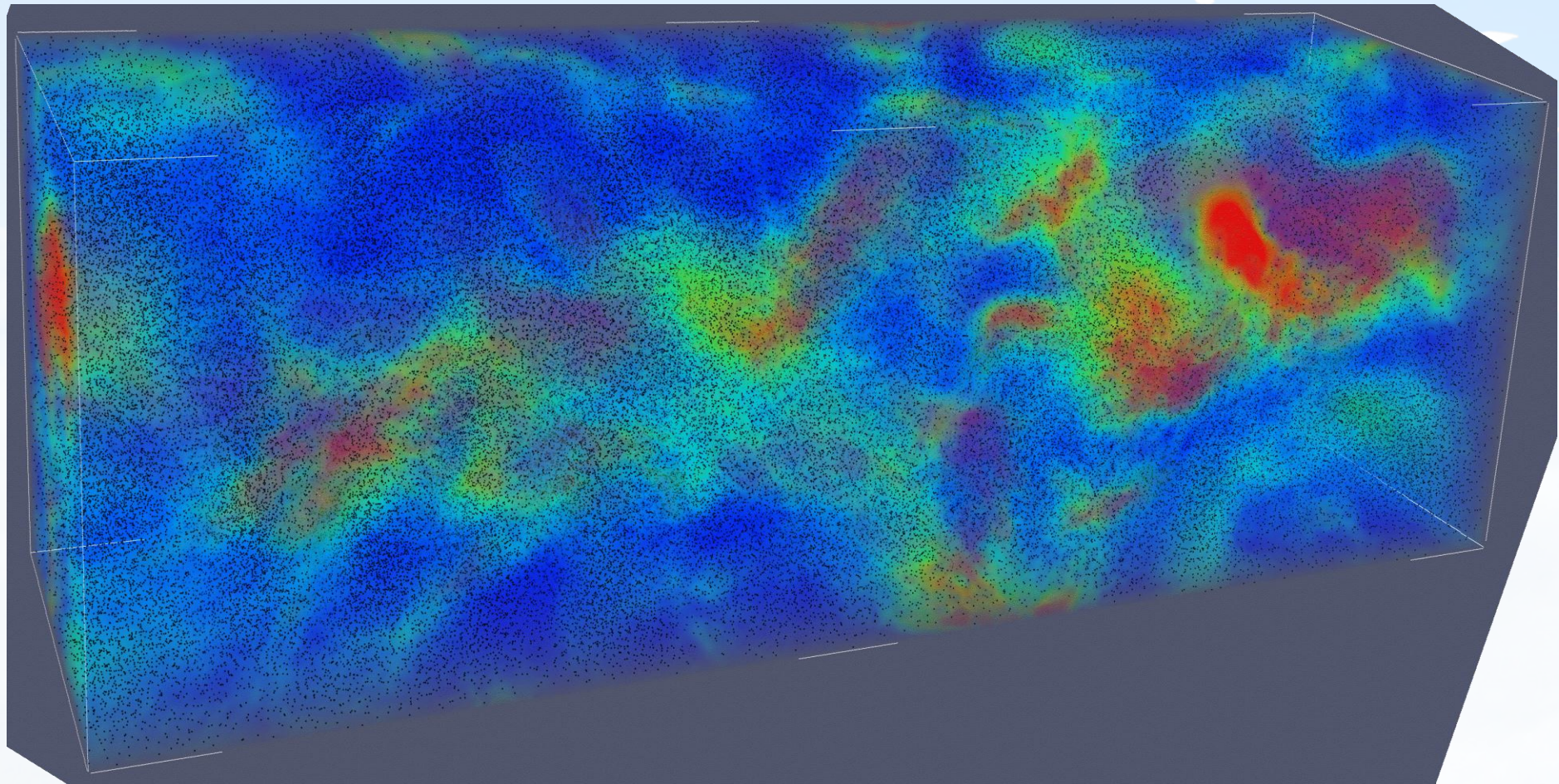
Others' DNS, such as  
*AIChE J.* 2013,59, 316-324.  
**10<sup>2</sup> Ps, 10<sup>5</sup> meshes**







# 130K solid particles in 3D @ 224 GPUs



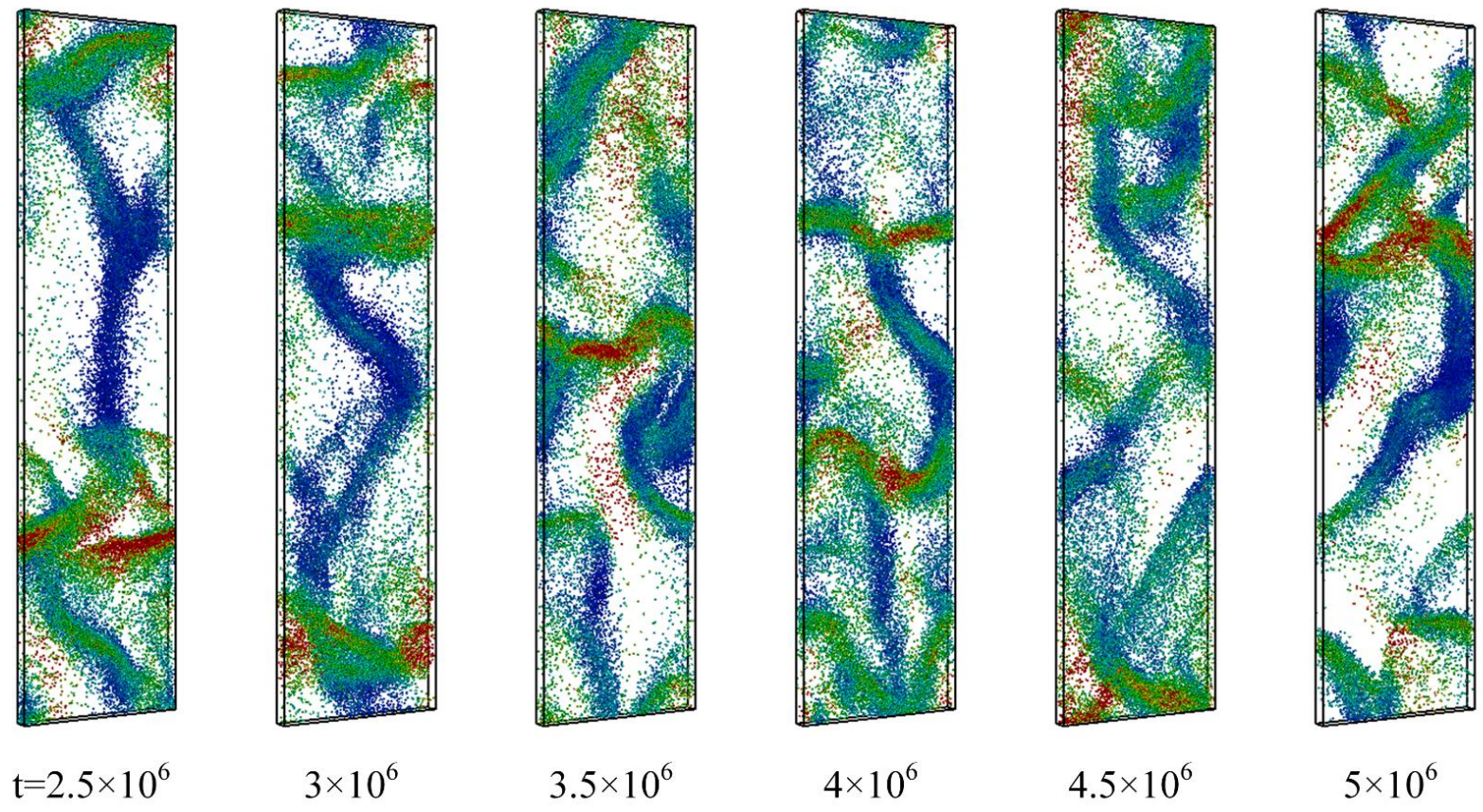
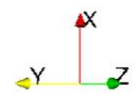
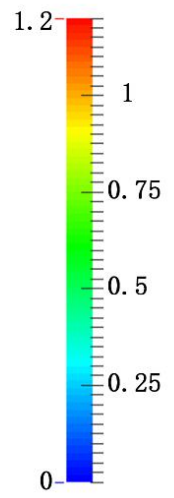
**3D: 0.384cm x 1.536cm x 0.384cm, 130000 particles ( 512 X 2560 X 512)**



# Snapshots for 3D DNS and Drag Distribution

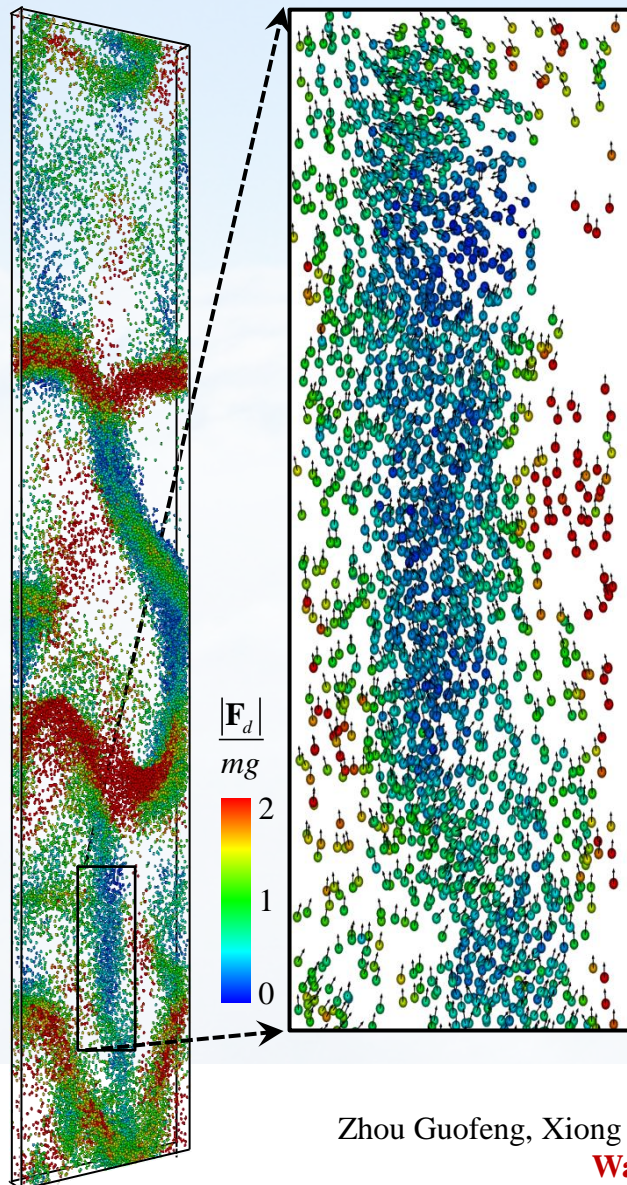


Force Magnitude

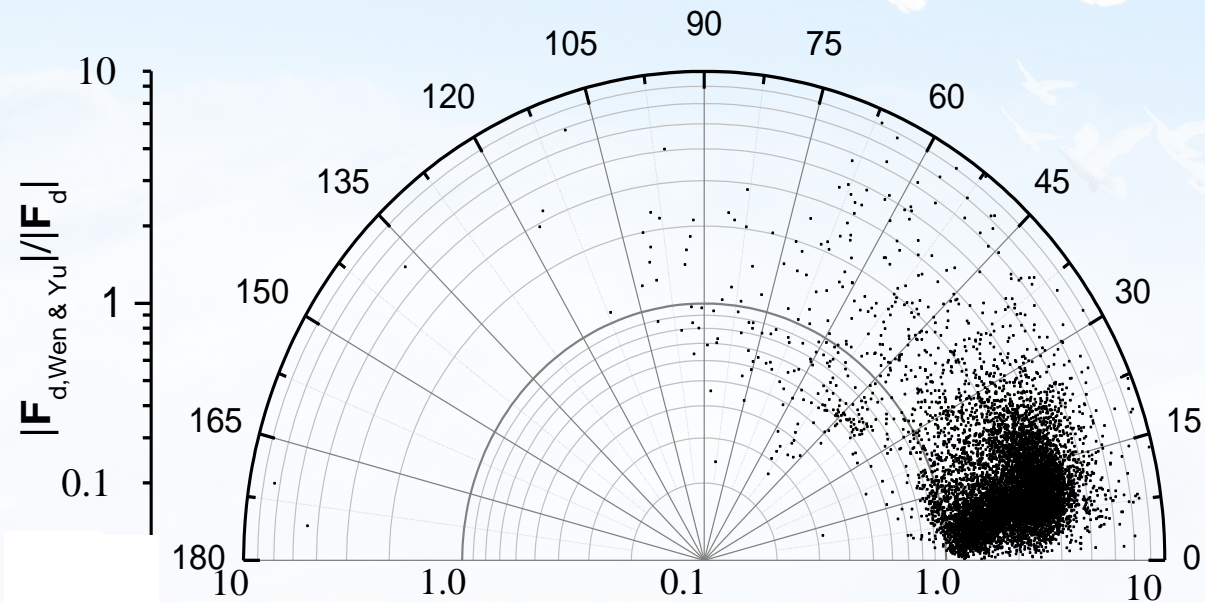




# Effect of Mesoscale Structure on Drag



$$\mathbf{F}_{g \leftrightarrow s, i} = \beta \cdot (\mathbf{u}_g - \mathbf{u}_s)$$

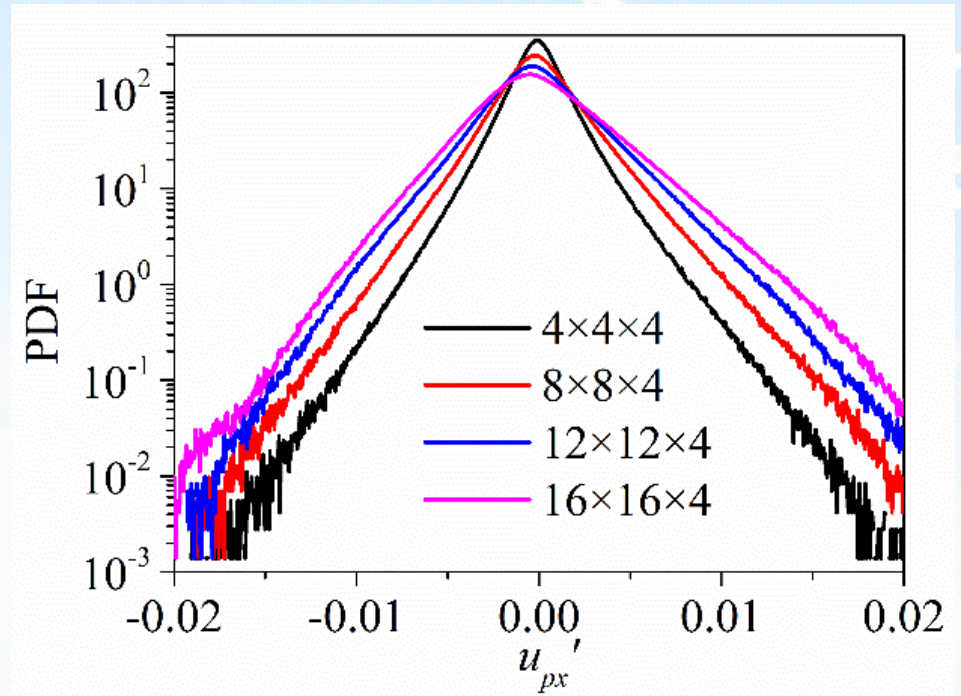
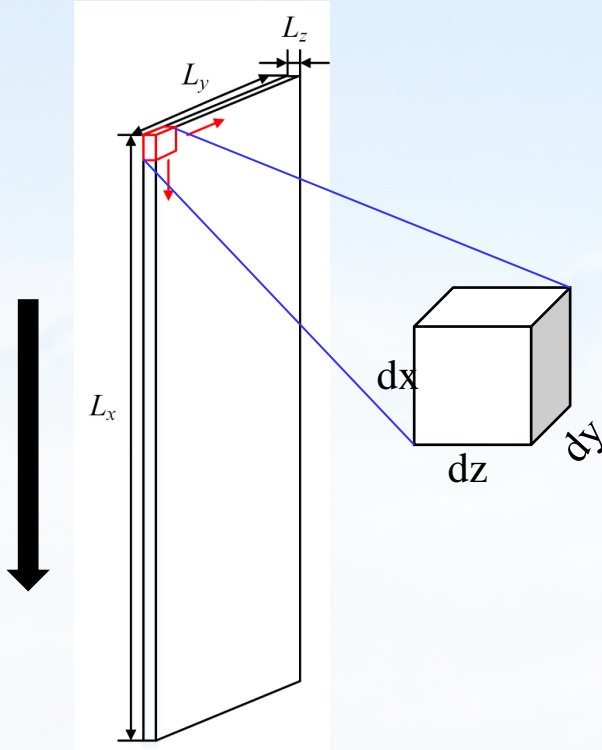


$$\beta \cdot (\mathbf{u}_g - \mathbf{u}_s) \approx \beta \mathbf{I} \cdot (\mathbf{u}_g - \mathbf{u}_s) = \beta (\mathbf{u}_g - \mathbf{u}_s)$$



# Scale-dependence of Domain Size

External force field



Fluctuating velocity distribution

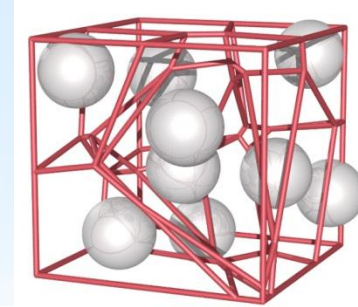
Granular Temperature

Sampling box	$\Theta_x$	$\Theta_y$	$\Theta_z$	$\Theta$
$4 \times 4 \times 4$	$3.21 \times 10^{-6}$	$2.61 \times 10^{-6}$	$1.68 \times 10^{-6}$	$2.50 \times 10^{-6}$
$8 \times 8 \times 4$	$5.85 \times 10^{-6}$	$4.23 \times 10^{-6}$	$1.74 \times 10^{-6}$	$3.94 \times 10^{-6}$
$12 \times 12 \times 4$	$8.96 \times 10^{-6}$	$5.98 \times 10^{-6}$	$1.76 \times 10^{-6}$	$5.57 \times 10^{-6}$
$16 \times 16 \times 4$	$1.25 \times 10^{-5}$	$7.56 \times 10^{-6}$	$1.77 \times 10^{-6}$	$7.28 \times 10^{-6}$

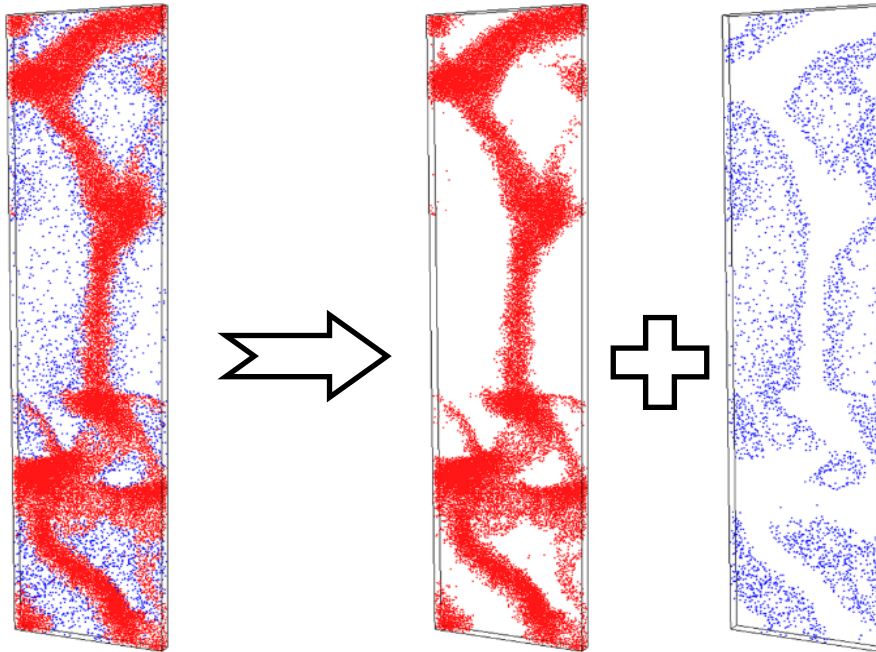
# Effect of Mesoscale Structure on Statistical Properties of Particles

Fluctuating velocity of particle  $i$  at  $j$  direction

$$u'_{i,j} \begin{cases} \overline{u_{i,j} - u_{dilute,j}} \\ \overline{u_{i,j} - u_{dense,j}} \end{cases}$$

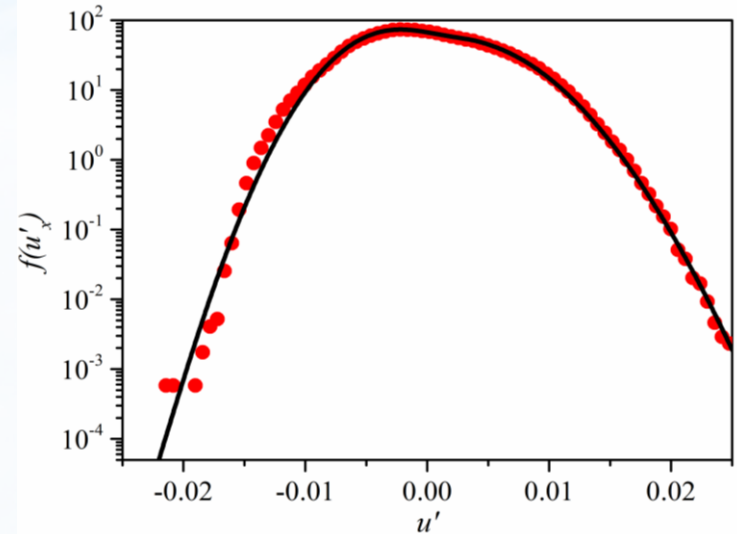


Voronoi tessellation



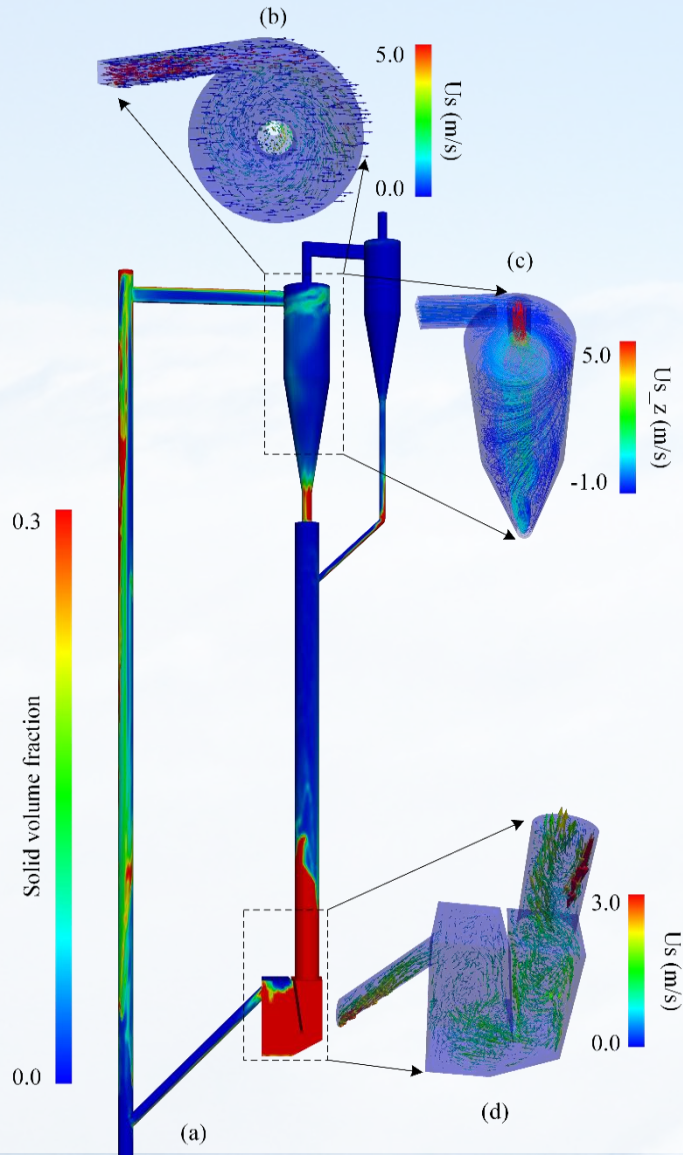
Dense phase

Dilute phase

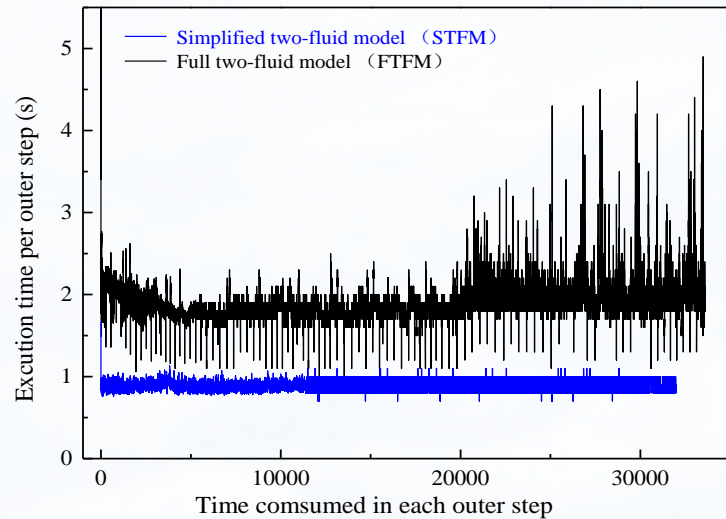
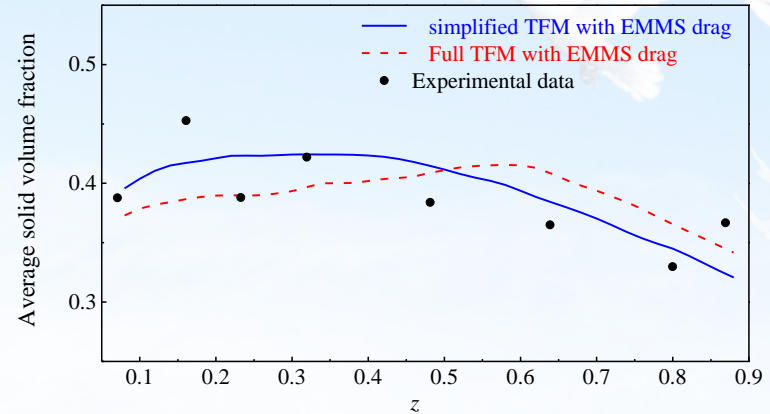


$$f(u'_x) = A_1 \exp\left(-\left|\frac{(u'_x - b_1)}{\sqrt{u'^2_{dilute,x}}}\right|^{1.8}\right) + A_2 \exp\left(-\left|\frac{(u'_x - b_2)}{\sqrt{u'^2_{dense,x}}}\right|^2\right)$$

# Simplified TFM with EMMS Drag



Prediction of STFMs coupled with EMMS drag also agrees with experimental data.



Simplified TFM is 2.14 times faster than full TFM!

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# Conclusions

Presented gas-solid statistical analysis of where we have used three strategies for enabling large-scale DNS including:

- A LBM-based DNS algorithm is proposed to simulate gas-solid flow
- LBM-DEM algorithm is feasible to be implemented on GPU
- Large-scale DNS of gas-solid flow has been efficiently run on GPU cluster
- The effects of mesoscale structure on both drag and statistical properties of particles were explored

Further investigations needed in constitutive laws (drag, solid stress, transfer of heat and mass, chemical reactions)

Better ways to link resolved models to coarse-grid simulation

# Acknowledgements

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